

# IWA TG on Benchmarking of Control Strategies for WWTPs

## The Quest for Objective Control Performance Evaluation

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## Outline

- Motive
- Background
- Benchmark systems
- Software platforms
- Outcome from Task Group

## Task Group members

- Dr Ulf Jeppsson, Lund Univ., Sweden (chair)
- Prof. P. Vanrolleghem, Univ. Laval, Canada (vice-chair)
- Dr John Copp, Primodal Inc., Canada
- Dr Marie-Noëlle Pons, CNRS-ENSIC-INPL, France
- Prof. Jean-Philippe Steyer, INRA, France
- Dr Christian Rosen, Lund Univ., Sweden
- Dr Jens Alex, IFAK, Germany
- Dr Krist Gernaey, Tech. Univ. of Denmark
- + 10-20 associated senior researchers world-wide

## Fundamental concept

Model simulations represent a relevant way to evaluate performance of control strategies for WWTPs

- Low cost
  - Safe
  - Fast
  - Include process, actuator and sensor problems
  - Effects of varying influent characteristics
- and much more ...

## Motive

A large number of proposed control strategies for WWTPs have been described. The available information is normally too limited to allow for detailed validation by other groups. Instead these strategies remain paper products. How can we promote the validation process, and thereby be able to compare the potential benefits of proposed strategies for a general WWTP and enhance their practical use?

Answer: **the Benchmark Simulation Protocol!**

## Benchmark simulation protocol?

- General WWTP layout
- Mathematical process models
- Influent wastewater characteristics
- Sensor and actuator models
  - Allow for users to provide control strategies
- Simulation procedures
- Criteria and tools for performance evaluation
  
- Provide software
- Promote plant-wide/integrated control and flexible solutions

## Background

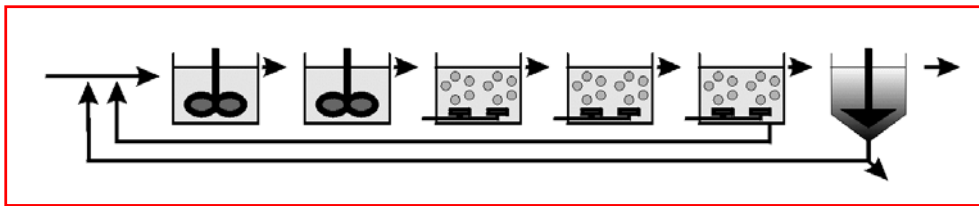
- Initial work started in 1997 within EU COST Actions 682&624 and IWA TG on Respirometry
- Basically the same research team today
- Task Group approved by IWA in October 2005
- Supported by IWA ICA and SAIA specialist groups
  
- Benchmark models used by >50 groups world-wide
- 100-200 papers at int. conferences and journals

## Benchmark systems

- No specific national or regional preferences
- Based on 'accepted' models, e.g. ASM1, ADM1, 10-layer 1-D settler model
- Fully dynamic including noise
- Allow for high flexibility of control
- Reasonable input and plant behaviour – focus is on *relative comparison of control strategies*
- Evaluation periods – one week or one year

# Benchmark Simulation Model no1 (BSM1)

- Models, benchmarking procedure and evaluation criteria
- Five-reactor AS plant with secondary clarification
- Sensor classes and noise defined, ideal actuators
- Three weather scenarios (dry, storm, rain)
- Performance during one week evaluated



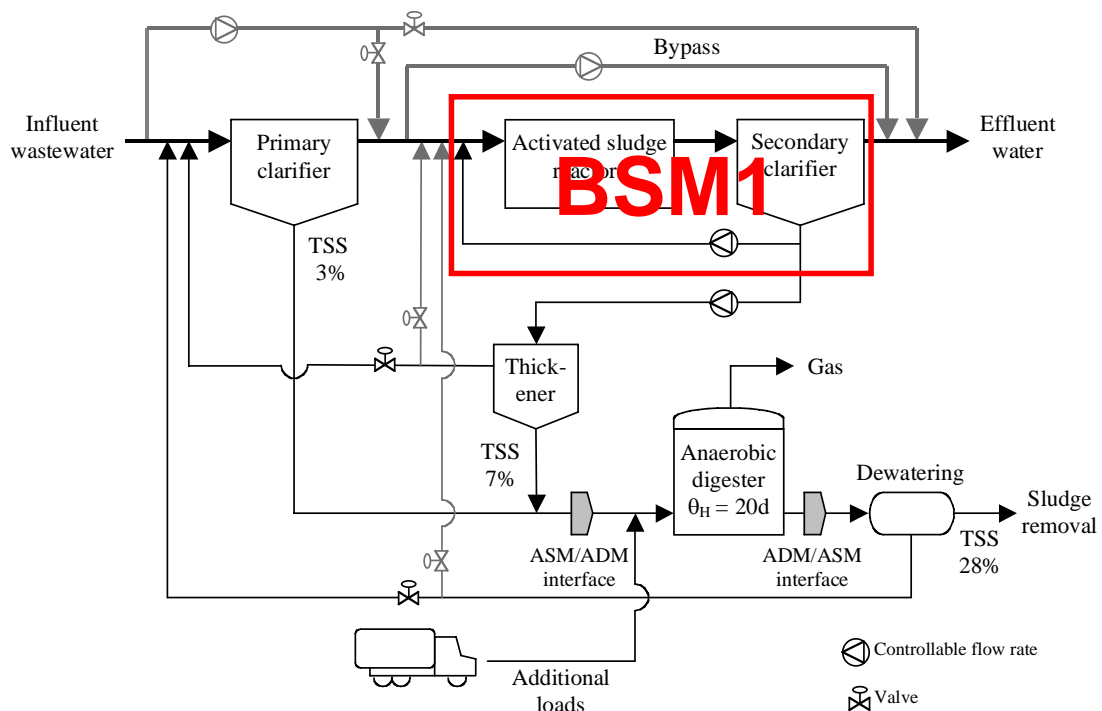
# BSM1 Long-Term (BSM1\_LT)

The original BSM1 configuration extended with:

- One year dynamics for evaluation period
- Influent wastewater generation model
- Time (temperature) varying parameters
- Sensor and actuator failures and disturbances
- Process faults and disturbances
- Additional actuators with long-term effects
- Focus on process monitoring
- Different evaluation criteria

# Benchmark Simulation Model no2 (BSM2)

- BSM1 and BSM1\_LT allow only for local control (monitoring) of an AS system
- Need for plant-wide ("within-fence") evaluation
- Importance of the sludge train
- Allow for supervisory long-term strategies
- Include full plant process interactions
- Avoid sub-optimisation
- Seasonal and holiday effects (also in BSM1\_LT)
- Generalization of influent generation (also in BSM1\_LT)



## Benchmark Simulation Model no2 (BSM2)

- One year dynamics for evaluation period
- ASM/ADM/ASM interfaces developed
- About 60 control handles available
- All realistic sensors possible, defined by classes:
  - Noise level, drift, time response and delay, calibration and maintenance requirements, lower & upper limits, measuring interval
- Allows for measurements from 'lab analyses'
- Considerable efforts to enhance simulation speed

## Evaluation criteria

- Effluent quality index (BOD, COD, TSS, TKN, NO<sub>3</sub>)
- Operational cost index based on:
  - Aeration energy
  - Pumping energy
  - Sludge production for disposal
  - External carbon
  - Mixing energy
  - Methane production (BSM2 only)
  - Heating energy (BSM2 only)
- Effluent limit violations, 95-percentiles and more
- Specific controller criteria (e.g. wear-and-tear)
- Possibly also a risk index (e.g. foaming, bulking, rising sludge)

## Software platforms

Development in parallel on:

- Matlab<sup>®</sup>/Simulink<sup>®</sup>
- WEST<sup>™</sup>
- SIMBA<sup>™</sup>
- GPS-X<sup>™</sup>
- Standalone FORTRAN

Possibly: standalone C, SciLab, STOAT, JASS, BioWin

## Outcome from Task Group

- Protocol for objective benchmarking of control and process monitoring strategies
- Available "free" software for several platforms
- Workshops (IWA2006, Watermatex2007, IWA2008)
- IWA Scientific and Technical Report (end of 2008)





# Thank You for Your Attention!

## Questions and comments?